

# Turbulence Deposition

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## Outline

- ▶ Semi-Empirical Models
- ▶ Free Flight Models
- ▶ Flow Structure Models
- ▶ Sublayer/Burst Models
- ▶ Deposition on Rough Walls

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Papavergos and Hedely (1984)

Vertical Channel

$$\tau^+ < 0.2$$

$$u_D^+ = 0.065 S_c^{-2/3}$$

$$0.2 < \tau^+ < 20$$

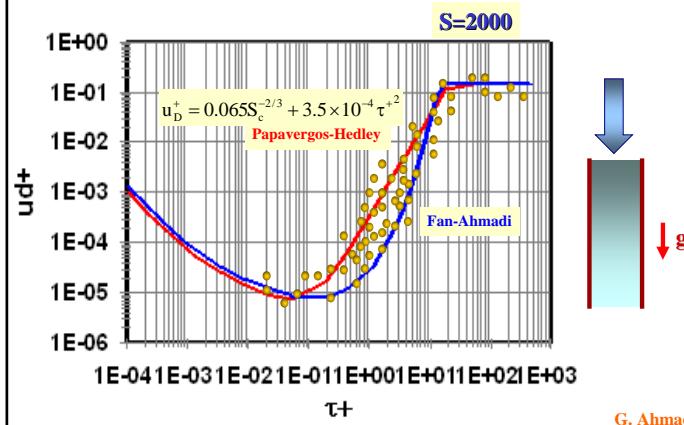
$$u_D^+ = 3.5 \times 10^{-4} \tau^{+2}$$

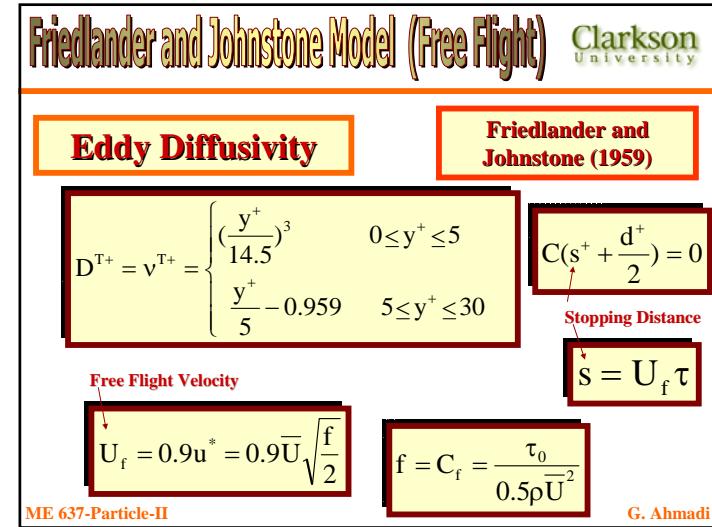
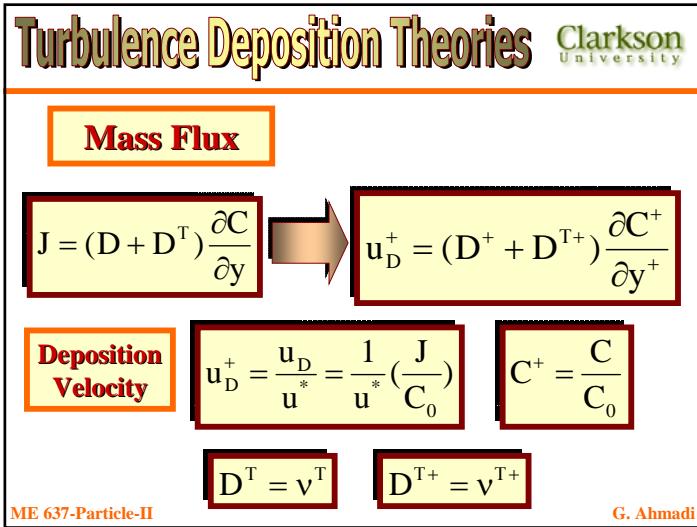
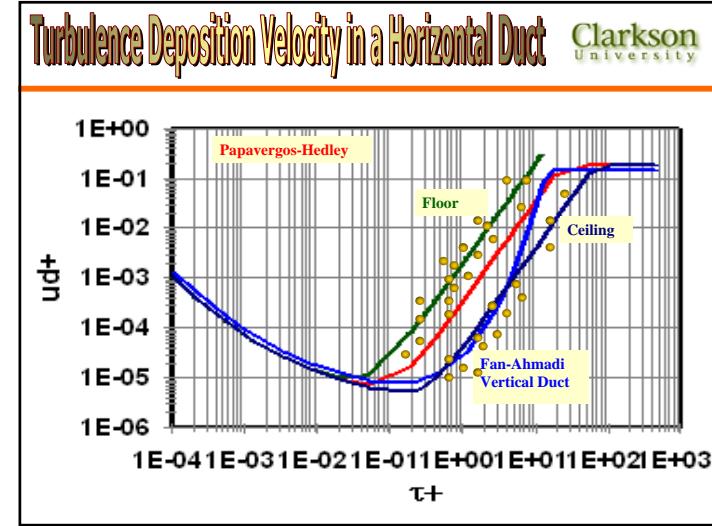
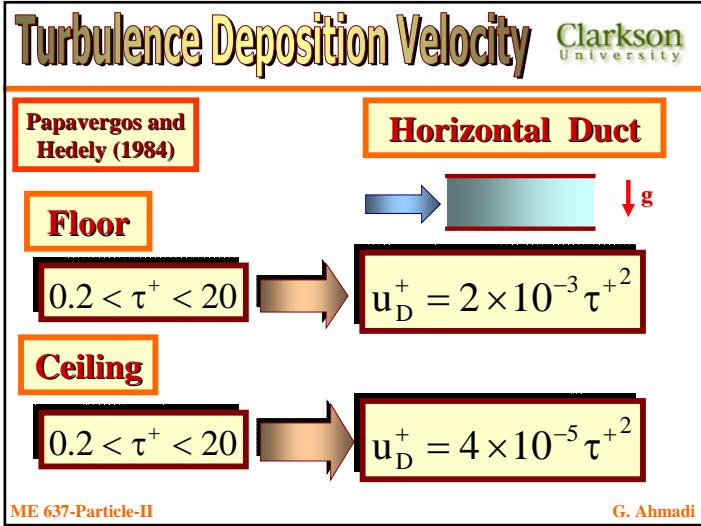
$$\tau^+ > 20$$

$$u_D^+ = 0.18$$

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## Friedlander and Johnstone Model

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### Deposition Velocity

$$u_d^+ = \left( \frac{1}{\sqrt{f/2}} + \frac{1525}{s^+} - 50.6 \right)^{-1} \quad s^+ \leq 5$$

$$u_d^+ = \left[ \frac{1}{\sqrt{f/2}} - 13.75 + 5 \ln \left( \frac{5.04}{0.5s^+ - 0.959} \right) \right]^{-1} \quad 5 \leq s^+ \leq 30$$

$$u_d^+ = \sqrt{f/2} \quad s^+ \geq 30$$

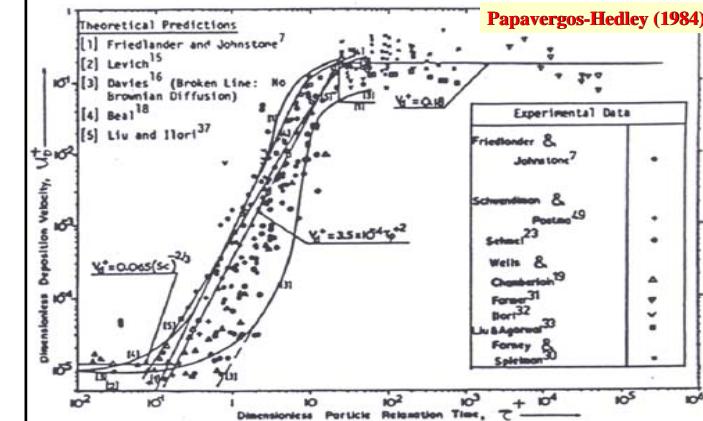
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$$s^+ = 0.9\tau^+$$

## Turbulence Deposition Theories

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Papavergos-Hedley (1984)

## Free Flight Deposition Models

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Levich (1962)

$$v^T \sim y^+^4$$

$$u_D^+ = 0.13337 S_c^{-3/4}$$

Davies

$$u_D^+ = 0.057 S_c^{-2/3}$$

Sehmel

$$D^{T+} = 0.011(y^+)^{1.1}(\tau^+)^{1.1} \quad y^+ < 20$$

$$U_f^+ = 1.49(\tau^+)^{-0.49}$$

$$D^{T+} = 0.04y^+ \quad y^+ > 20$$

Liu and Ilory

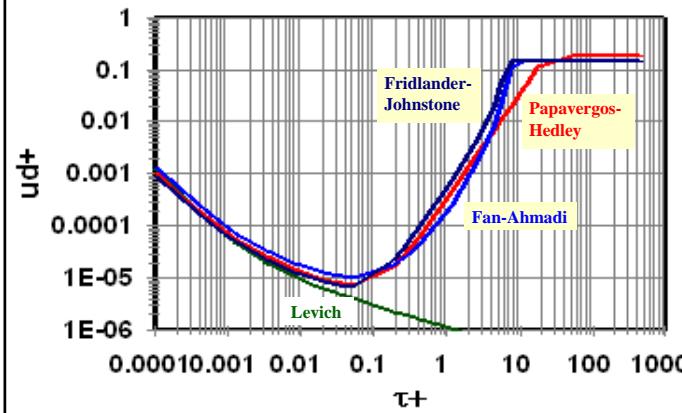
$$D^{T+} = v^T + \left( \frac{y^+}{y^+ + 10} \right)^2 \tau^+$$

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## Comparisons of Turbulence Deposition Model

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Fridlander-Johnstone

Papavergos-Hedley

Fan-Ahmadi

Levich

## Limitations of Free-Flight Models

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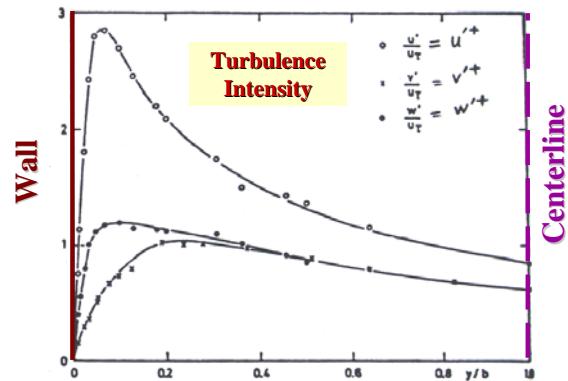
- Use of the concept of 'stopping distance' as a sink boundary condition for particle
- Assumptions for free-flight velocity
- Equality of particle mass diffusivity to the turbulence eddy diffusion.
- Ignoring the effects of density ratio, Reynolds number, and scales of turbulence.
- Ignoring the effects of lift force.
- Ignoring the effects of coherent eddies and bursting phenomena.

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## Structure of Turbulence Near a Wall

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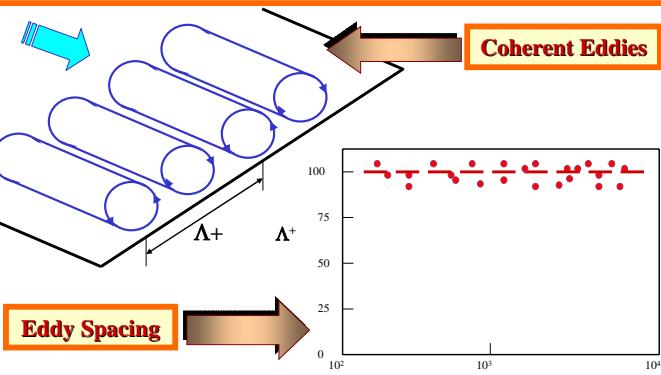


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## Streaky Wall Flow

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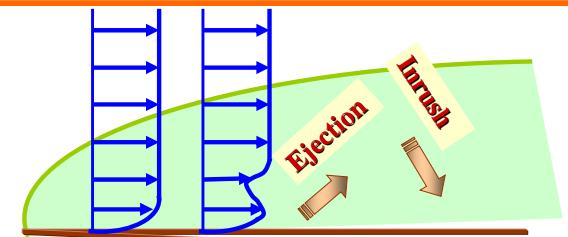


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## Bursting Phenomena

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Time Between Bursts

$$T_B^+ = 0.65 R_\theta^{0.73}$$

$$\frac{V_0 T_B}{\delta} \approx 5$$

Bursts Duration

$$0.25 T_B$$

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# Cleaver and Yates Model

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- Suspended particles diffuse to a certain distance from the wall by turbulent diffusion before being entrained in a down-sweep.
- The flow in a down-sweep may be approximated as a two-dimensional stagnation-point flow in the sub-layer.
- Only Stokes drag is acting on the particles.

$$u_D^+ = \frac{9}{400} \frac{\rho_f}{\rho_p} \tau^+ \exp\{0.48\tau^+\} + 0.084 Sc^{-2/3}$$

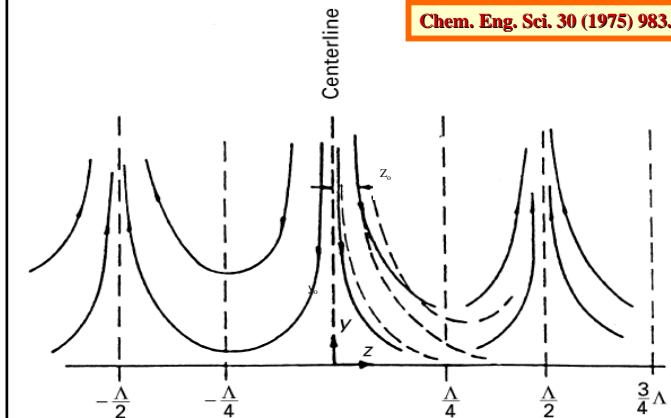
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# Cleaver-Yates Model

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Chem. Eng. Sci. 30 (1975) 983.



# Cleaver and Yates Model

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**Flux**  $\rightarrow J = C(y)v_0(y)A_c(y)$

**Deposition Velocity**  $\rightarrow u_D^+ = \frac{J}{Cu^*} = \frac{v_0^+ A_c}{2}$

**Equation of Motion**  $A_c - \text{capture area ratio} = \frac{z_0}{\Lambda}$

$$\tau^+ \frac{dv^+}{dt^+} = v^{f+} - v^+$$

$$\tau^+ \frac{dw^+}{dt^+} = w^{f+} - w^+$$

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# Cleaver and Yates Model

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## Perturbation Solution

$$v^+ = v^{f+} - \tau^+ \left( v^{f+} \frac{\partial v^{f+}}{\partial y^+} + w^{f+} \frac{\partial v^{f+}}{\partial z^+} \right)$$

## Flow Field

$$w^f = \alpha z \varphi'(\eta)$$

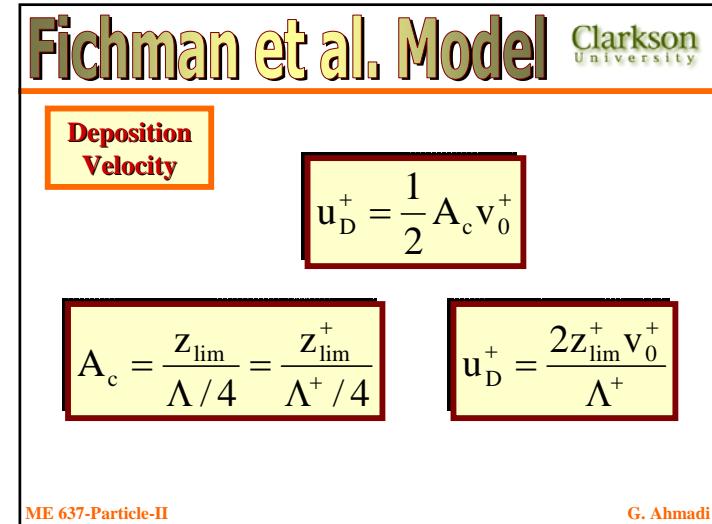
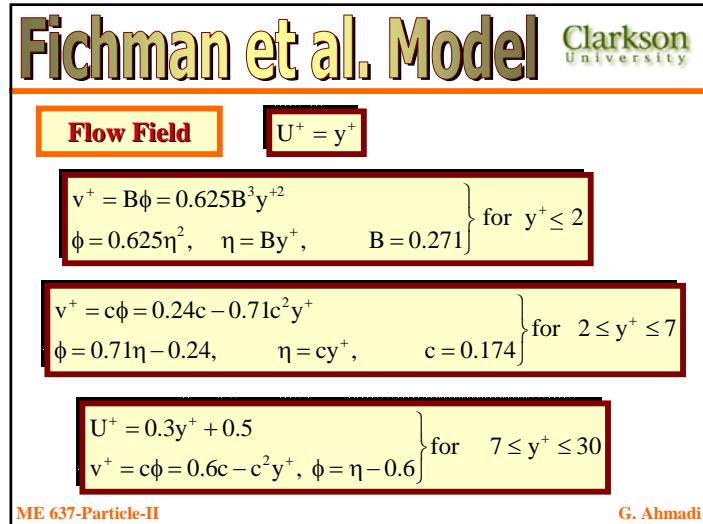
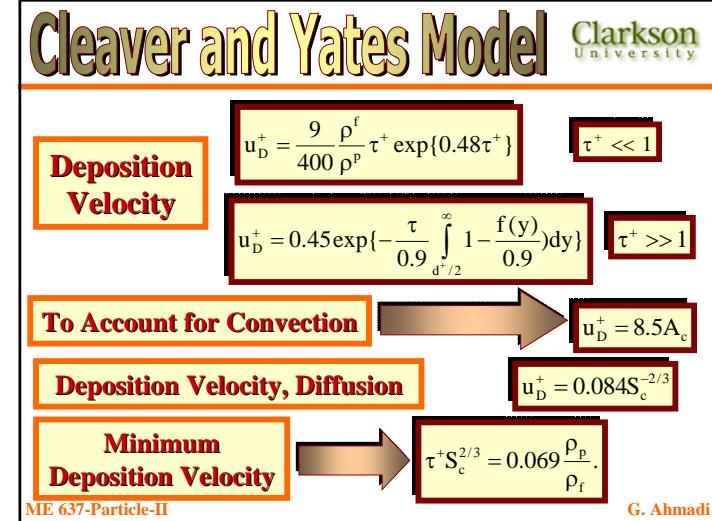
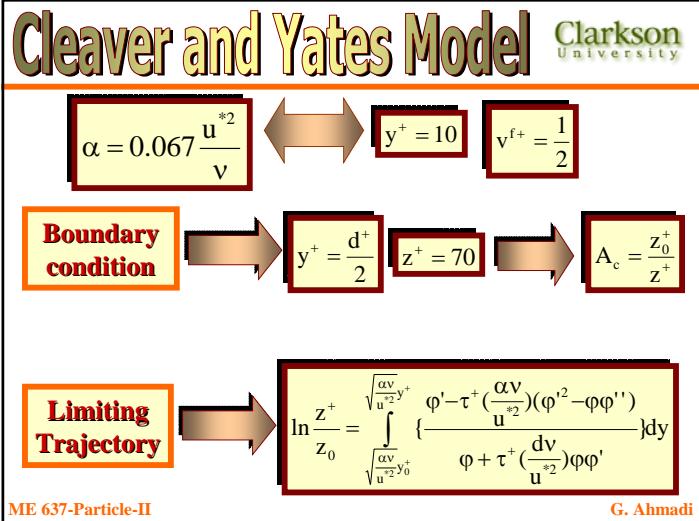
$$v^f = -\sqrt{\alpha v} \varphi(\eta)$$

$$\eta = \sqrt{\frac{\alpha}{v}} y$$

$$\varphi''' + \varphi \varphi'' - \varphi'^2 + 1 = 0$$

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## Fichman et al. Model

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### Equations of Motion

$$\tau^+ \frac{d^2 x^+}{dt^{+2}} = U^+ - \frac{dx^+}{dt}$$

$$\tau^+ \frac{d^2 y^+}{dt^{+2}} = v^+ - \frac{dy^+}{dt} + K \left( U^+ - \frac{dx^+}{dt} \right)$$

$$\tau^+ \frac{d^2 z^+}{dt^{+2}} = w^+ - \frac{dz^+}{dt}$$

$$K = \tau^+ L^+$$

Lift

$$L^+ = \frac{Lv}{u^{*2}}$$

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## Fichman et al. Model

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Lift

$$L \approx \frac{6.46\mu \left(\frac{d}{2}\right)^2}{v^{1/2} m_p} \left(\frac{dU}{dy}\right)^{1/2} = \frac{3.08\mu \dot{\gamma}^{1/2}}{v^{1/2} d\rho_p} \quad \dot{\gamma} = \frac{dU}{dy}$$

$$\frac{4z_{lim}^+}{\Lambda^+} = \frac{d^2}{4} + (d^+ + s^+) \dot{s}^+$$

$$s^+ \leq 2$$

$$s^+ = \frac{L^+ \tau^{+2} (u_{po}^+ - \dot{\gamma}^+ y_0^+) + \tau^+ v_{po}^+}{1 - \tau^{+2} L^+ \dot{\gamma}^+}$$

Numerical Solution

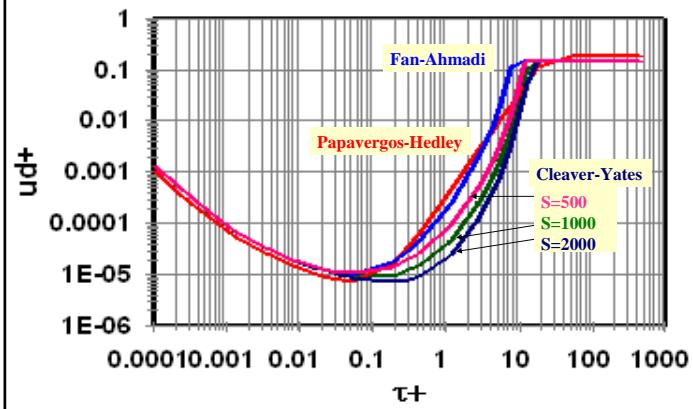
$$s^+ \geq 2$$

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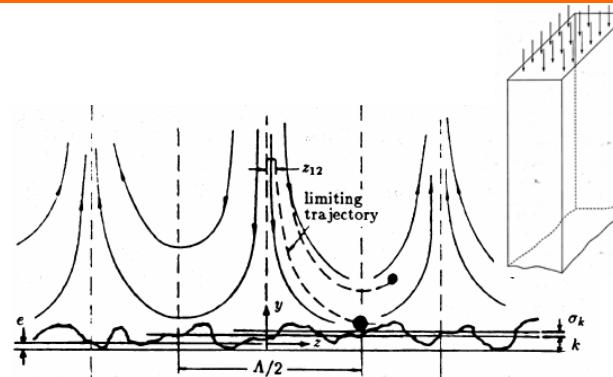
## Cleaver and Yates Model

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## Fan-Ahmadi Model

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# Fan-Ahmadi Model

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# Equations of Motion

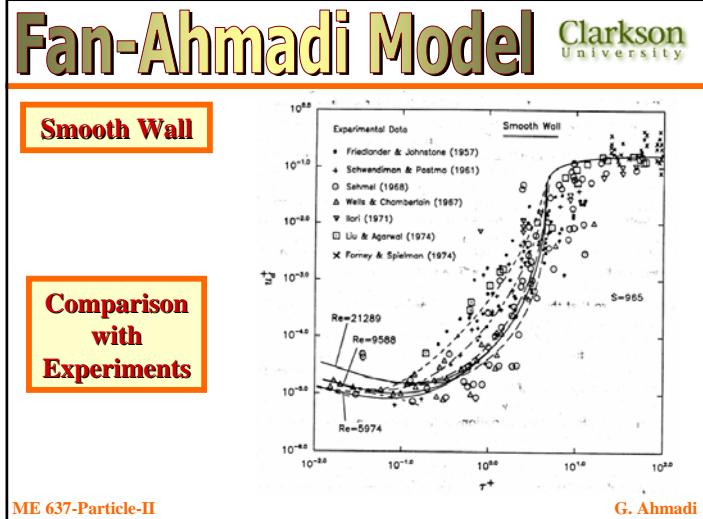
$$\tau^+ \frac{du^{p+}}{dt^+} = u^+ - u^{p+} + \tau^+ g^+,$$

$$\tau^+ \frac{dv^{p+}}{dt^+} = v^+ - v^{p+} + \tau^+ L_1^+(u^+ - u^{p+}) + \tau^+ L_2^+(w^+ - w^{p+}),$$

$$\tau^+ \frac{dw^{p+}}{dt^+} = w^+ - w^{p+},$$

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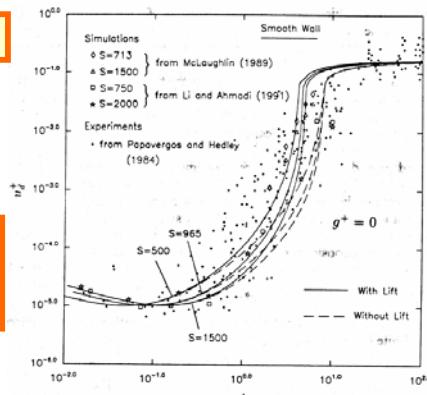
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# Fan-Ahmadi Model

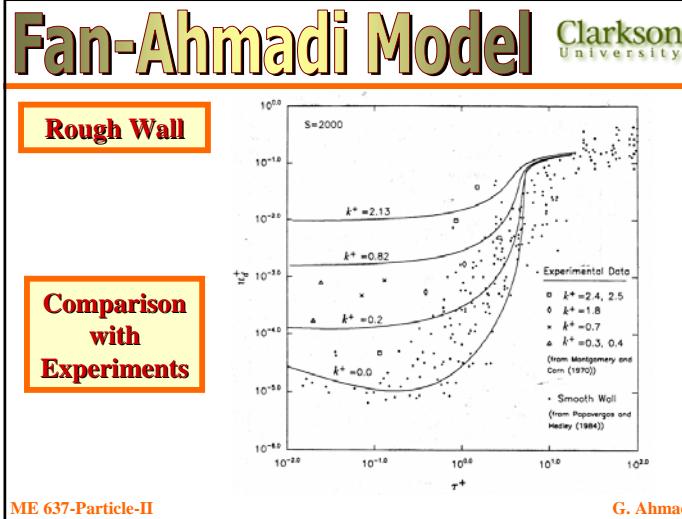
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## **Smooth Wall**



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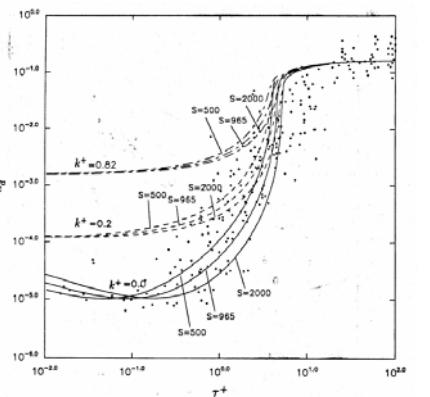
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# Fan-Ahmadi Model

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## Rough Wall

### Effects of Density Ratio



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# Deposition Velocity for Rough Walls

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## Fan and Ahmadi

## Empirical Model

$$u_d^+ = \begin{cases} 0.084Sc^{-2/3} + \frac{1}{2} \left[ \frac{\left(0.64k^+ + \frac{d^+}{2}\right)^2 + \frac{\tau_p^{+2}g^+L_1^+}{0.01085(1+\tau_p^{+2}L_1^+)} }{3.42 + \frac{\tau_p^{+2}g^+L_1^+}{0.01085(1+\tau_p^{+2}L_1^+)} } \right]^{1/(1+\tau_p^{+2}L_1^+)} & \text{if } u_d^+ < 0.14 \\ \times \left[ 1 + 8e^{-(\tau_p^+-10)^2/32} \right] \frac{0.037}{1 - \tau_p^{+2}L_1^+(1 + \frac{g^+}{0.037})} & \text{otherwise} \\ 0.14 & \end{cases}$$

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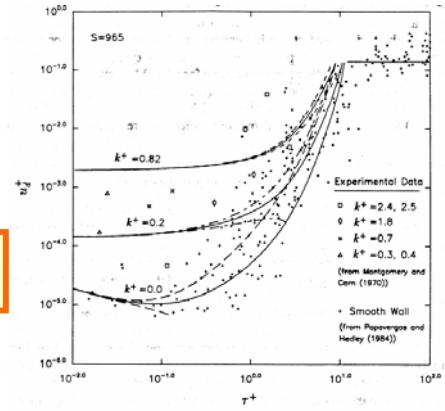
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# Fan-Ahmadi Model

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## Rough Wall

### Empirical Model Predictions



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# Concluding Remarks

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- ▶ Semi-Empirical Models
- ▶ Free Flight Models
- ▶ Flow Structure Models
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