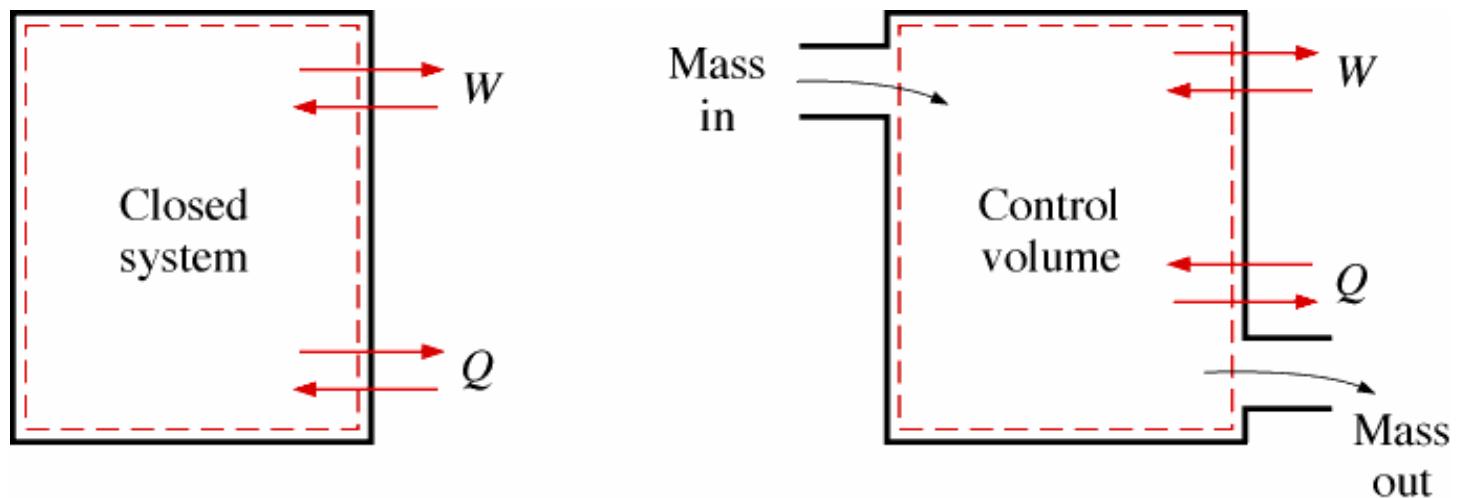


# Control Volume Analysis Using Energy

# Open vs. Closed Systems

Session-8



# Conservation of Mass

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- In a closed system the mass is always constant
- In an open system (control volume) we need to consider mass balance

$$\begin{array}{c} \text{Sum of the rate} \\ \text{of mass} \\ \text{flowing into the} \\ \text{control volume} \end{array} - \begin{array}{c} \text{Sum of the rate} \\ \text{of mass flowing} \\ \text{from the control} \\ \text{volume} \end{array} = \begin{array}{c} \text{Time rate of} \\ \text{change of the} \\ \text{mass inside the} \\ \text{control volume} \end{array}$$

$$\sum m_{in} - \sum m_{out} = \Delta m_{cv}$$

$$\sum \dot{m}_{in} - \sum \dot{m}_{out} = \frac{dm_{cv}}{dt}$$

# Calculating The Flow Rate

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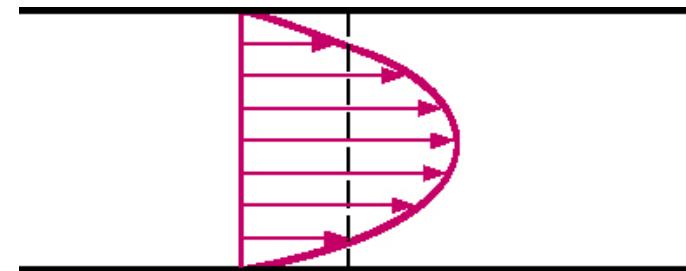
$$\dot{m} = \rho \vec{V} \cdot \vec{A} = \frac{\vec{V} \cdot \vec{A}}{v}$$

Volumetric Flow Rate

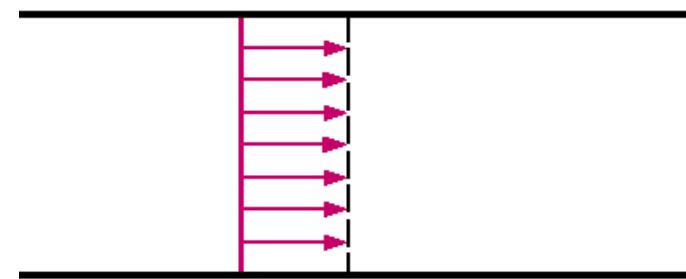
$$\dot{V} = \vec{V} \cdot \vec{A}$$

$$\dot{m} = \rho \dot{V} = \frac{\dot{V}}{v}$$

General Formula



(a) Actual



(b) Average

$$\dot{m} = \int_{\vec{A}} \rho \vec{V} \cdot d\vec{A} = \int_{\mathcal{V}} \rho d\mathcal{V}$$

The total amount of mass in the control volume does not change with time

$$\sum m_i = \sum m_e$$

$$\sum \dot{m}_i = \sum \dot{m}_e$$

## First Law of Thermodynamics

$$\sum E_i - \sum E_e = \Delta E_{cv}$$

$$\sum \dot{E}_i - \sum \dot{E}_e = \frac{dE_{cv}}{dt}$$

## Total Energy of a flowing fluid

$$e = u + ke + pe = u + \frac{V^2}{2} + gz$$

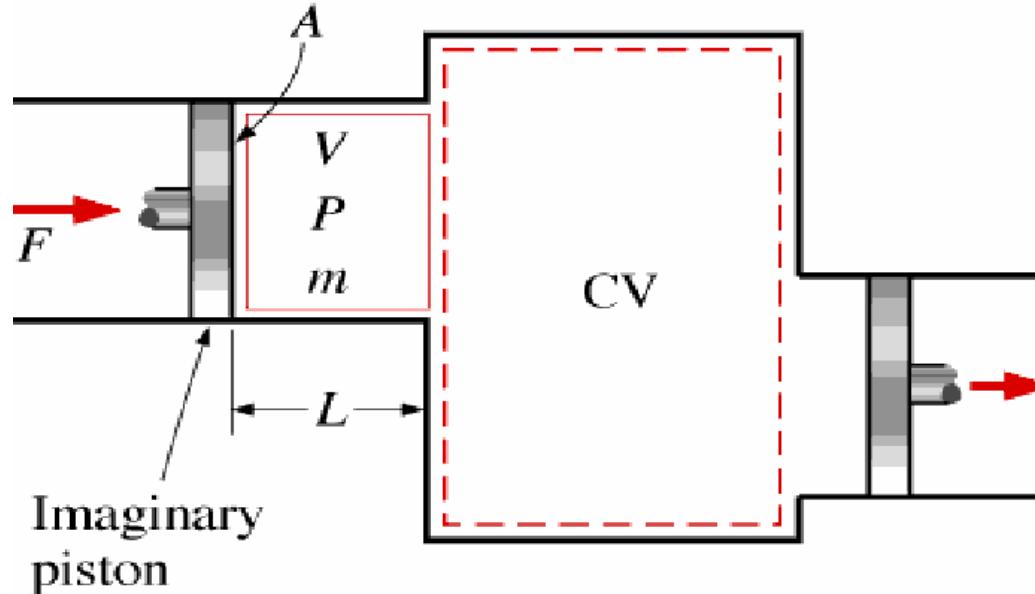
$$\frac{dE_{cv}}{dt} = \sum \dot{Q} - \sum \dot{W} + \sum \dot{m}_i \left( u_i + \frac{V_i^2}{2} + gz_i \right) - \sum \dot{m}_e \left( u_e + \frac{V_e^2}{2} + gz_e \right)$$

# Flow Work

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It takes work to push a fluid into a system

It takes work to push a fluid out of a system



$$\dot{W}_{\text{flow}} = F \cdot \frac{\Delta x}{t} = (pA) \cdot \frac{\Delta x}{t} = pAV$$

$$\dot{W} = \dot{W}_{\text{cv}} + \underbrace{(p_e A_e)V_e - (p_i A_i)V_i}_{\dot{m}_e(p_e v_e)}$$

# Energy Balance

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$$\frac{dE_{cv}}{dt} = \sum \dot{Q}_{cv} - \sum \dot{W}_{cv} + \sum \dot{m}_i \left( u_i + p_i v_i + \frac{V_i^2}{2} + gz_i \right) - \sum \dot{m}_e \left( u_e + p_e v_e + \frac{V_e^2}{2} + gz_e \right)$$

or

$$\frac{dE_{cv}}{dt} = \sum \dot{Q}_{cv} - \sum \dot{W}_{cv} + \sum \dot{m}_i \left( h_i + \frac{V_i^2}{2} + gz_i \right)$$

$$- \sum \dot{m}_e \left( h_e + \frac{V_e^2}{2} + gz_e \right)$$

represents everything  
but the flow work

Mass Balance(Continuity):  $\dot{m}_{cv} = 0$

Energy Balance:

$$\frac{dE_{cv}}{dt} = 0$$

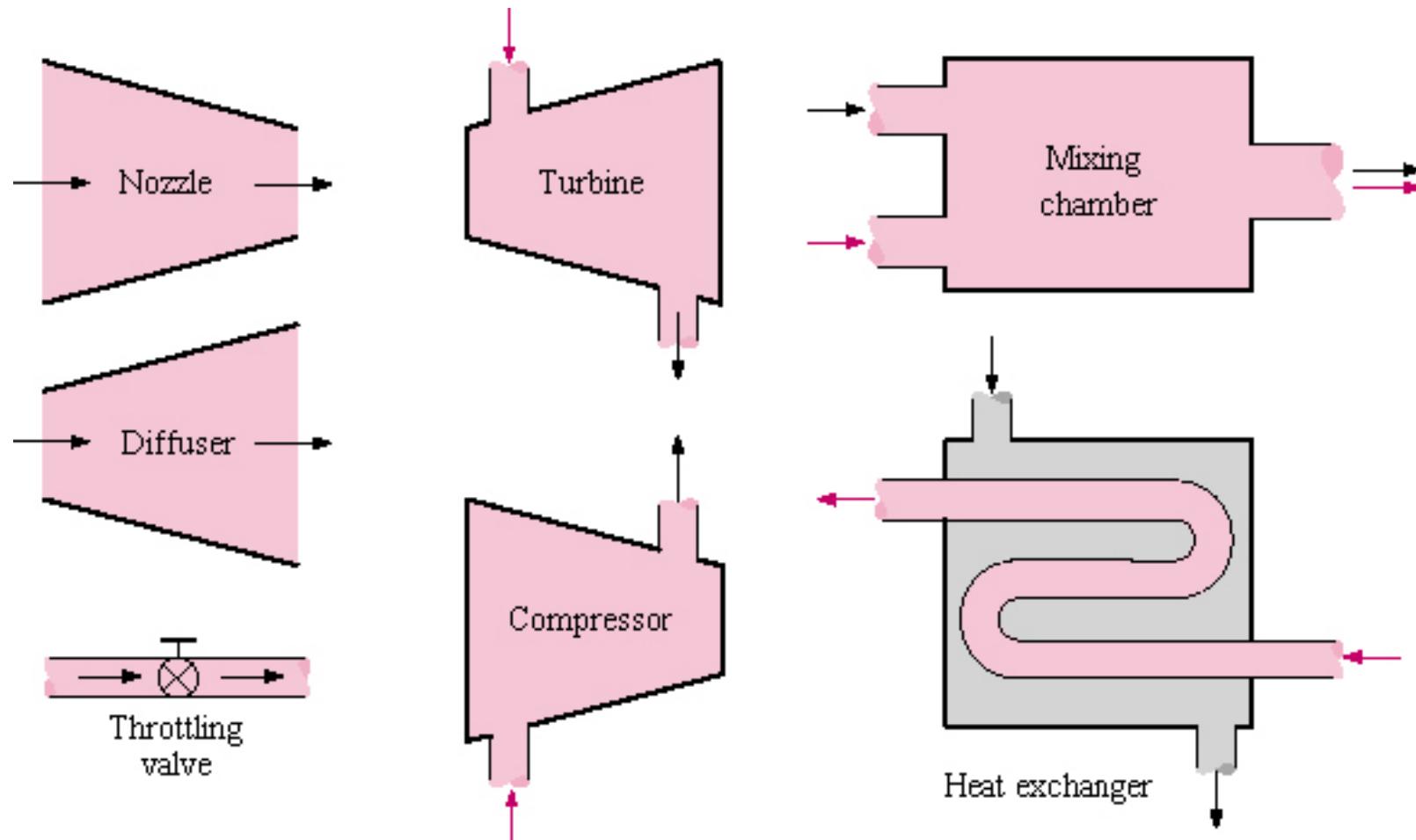
or

$$\sum \dot{m}_i = \sum \dot{m}_e$$

$$\dot{Q}_{net} - \dot{W}_{net} - \sum \dot{m}_e \left( h_e + \frac{V_e^2}{2} + gz_e \right) + \sum \dot{m}_i \left( h_i + \frac{V_i^2}{2} + gz_i \right) = 0$$

# Some Common Steady Flow Devices

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Nozzles

Diffusers

Turbines

Compressors

Throttling Valve

$$\dot{m}_i = \dot{m}_e = \dot{m}$$

$$\dot{Q} - \dot{W} = \dot{m} \left[ h_e - h_i + \frac{V_e^2 - V_i^2}{2} + g(z_e - z_i) \right]$$