

Name:

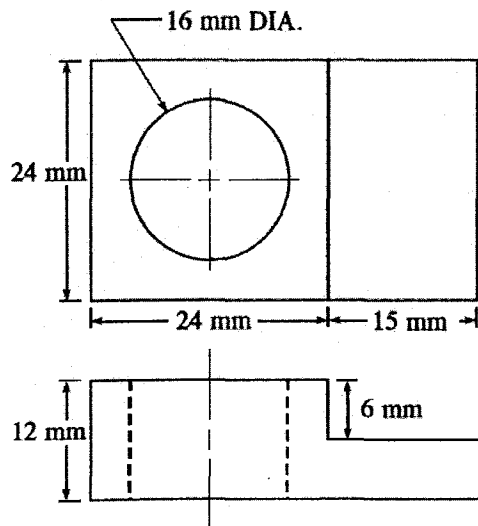
(1 Hour)

**Problem 1 (10 points):** A rod of length  $L$  has one end maintained at temperature  $T_0$  and is exposed to an environment at temperature  $T_\infty$ . An electrical heating element is placed in the rod so that heat is generated uniformly along the length at a rate  $\dot{q}$ . Derive an expression

- For the temperature distribution in the rod, (3 points)
- For the total heat transferred to the environment, (3 points)
- Obtain an expression for the value of  $\dot{q}$  that will make the heat transfer zero at the end which is maintained at  $T_0$ . (4 points)
- Bonus** If  $\dot{q} = a + b.x$ , find the expression for the temperature. (5 points)

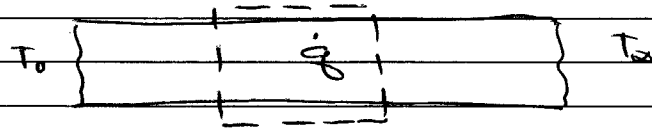
**Problem 2 (10 points):** The part shown below is machined from Stainless Steel ( $\rho=7978 \text{ kg/m}^3$ ,  $k=18.9 \text{ W/mK}$ ,  $C_p=559 \text{ J/kgK}$ ). When the part is removed from the heat treating furnace, it has an initial uniform temperature of  $600^\circ\text{C}$ . All surfaces of the part are exposed to a flow of coolant with a temperature of  $30^\circ\text{C}$  and a heat transfer coefficient of  $h=25 \text{ W/m}^2\text{K}$ .

- Check the validity of the lumped capacitance method for this problem. (3 points)
- Calculate how long it will take for the part to cool to  $54^\circ\text{C}$ . (4 points)
- When the part has a temperature of  $54^\circ\text{C}$ , what are the instantaneous rate of heat loss from the part and the instantaneous rate of cooling (in  $^\circ\text{C/s}$ ). (3 points)



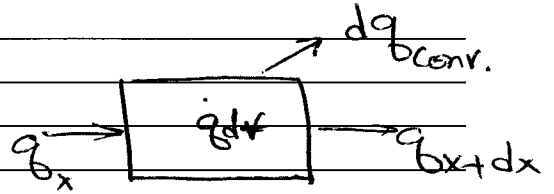
## Problem 1:

Similar to the example in the eKBS, we have



Energy Balance for

$$E_{in} - E_{out} = E_{st} \overset{\circ (S.S)}{\rightarrow} - E_{gen} \quad (1)$$



$$q_{x} - q_{x+dx} = -\dot{q} dx$$

$$q_x = -KA \frac{dT}{dx} \rightarrow \frac{dq_x}{dx} = -KA \frac{d^2T}{dx^2} \quad \text{for } K = \text{const.}$$

$$q_{conv.} = hA(T - T_\infty) \rightarrow dq_{conv.} = h dA(T - T_\infty)$$

plugging into Eq (1) and simplify

$$\frac{d^2T}{dx^2} - \frac{hP}{KA}(T - T_\infty) + \frac{\dot{q}}{K} = 0$$

or if  $\theta = T - T_\infty$

$$\theta'' - m^2 \theta + \frac{\dot{q}}{K} = 0, \quad m^2 = \frac{hP}{KA}$$

The solution to this differential equation (which is non-homogeneous but linear) is given

as

$$\theta = C_1 e^{mx} + C_2 e^{-mx} + \frac{\dot{q}}{m^2 K}$$

Prob. 1 / Cont'd

The boundary conditions are

$$\theta(0) = \theta_0 \quad \text{(a)} \quad , \quad -k \frac{d\theta}{dx} \Big|_{x=L} = h \theta \Big|_{x=L} = h \theta_L \quad \text{(b)}$$

using (a)

$$\theta_0 = c_1 + c_2 + \frac{q}{m^2 k}$$

using (b)

$$-c_1 e^{mL} + c_2 e^{-mL} = \frac{h \theta_L}{k m}$$

multiply by  $e^{mL} \rightarrow -c_1 e^{2mL} + c_2 = \frac{h \theta_L}{k m} e^{mL}$

Subtract from (a)  $\rightarrow c_1 = - \frac{\frac{q}{m^2 k} + \frac{h \theta_L}{k m} e^{mL} - \theta_0}{1 + e^{2mL}}$

or  $c_1 = \frac{[\frac{q}{m^2 k} - \theta_0] e^{-mL} + h \theta_L / k m}{e^{mL} + e^{-mL}}$

with a similar procedure & and using (a)

$$c_2 = \frac{e^{mL} (\theta_0 - \frac{q}{m^2 k}) + h \theta_L / k m}{e^{mL} + e^{-mL}}$$

Finally

$$\theta = \frac{e^{-mL} (\theta_0 - \frac{q}{m^2 k}) - h \theta_L / k m}{e^{mL} + e^{-mL}} + \frac{e^{mL} (\theta_0 - \frac{q}{m^2 k}) + h \theta_L / k m}{e^{mL} + e^{-mL}} + \frac{q}{m^2 k}$$

or using  $\cosh mL = \frac{e^{mL} + e^{-mL}}{2}$

$$\sinh mL = \frac{e^{mL} - e^{-mL}}{2}$$

# Problem 1 / Cont'd.

You can rewrite this equation

$$\theta = \frac{[\theta_0 - \dot{q}/m^2k] e^{-mL} e^{mx} + [\theta_0 - \dot{q}/m^2k] e^{mL} e^{-mx}}{2 \cosh(mL)}$$

$$+ \frac{h\theta_L/km [e^{mx} + e^{-mx}]}{2 \cosh(mL)} + \frac{\dot{q}}{km^2}$$

or

$$\theta = \frac{[\theta_0 - \dot{q}/m^2k] \underbrace{(e^{-m(L-x)} + e^{m(L-x)})}_{2 \cosh(m(L-x))}}{2 \cosh(mL)}$$

$$+ \frac{h\theta_L/km [2 \sinh mx]}{2 \cosh(mL)} + \frac{\dot{q}}{km^2}$$

or

$$\theta = \frac{[\theta_0 - \dot{q}/m^2k] \cosh(m(L-x)) - \frac{h\theta_L}{km} \sinh(mx)}{\cosh(mL)} + \frac{\dot{q}}{km^2}$$

Ans.

(b)

The total heat loss is due to convection and can be found from

$$dq_{conv.} = h dA_s \theta \Rightarrow q_{conv.} = q_{loss} = \int h A_s \theta$$

we need to include heat transfer from

the tip too, which is  $q_{tip} = h A_{tip} (\theta_L)$

So

$$\begin{aligned}
 \dot{q}_{\text{loss}} &= \int_0^L h dA_s \theta + h A_{\text{tip}} \theta_L \\
 &= \int_0^L h \overbrace{(P dx)}^{dA_s} \theta + h \overbrace{A_{\text{tip}}}^{A_{\text{conduction}} = \text{Across section}} \theta_L \\
 &= Ph \int_0^L \theta dx + h A_c \theta_L \\
 &= P \cdot b \int_0^L \frac{[\theta_0 - \dot{q}_0 / m^2 k] \cosh(m(L-x)) - \frac{h \theta_L}{k m} \sinh(mx)}{\cosh(mL)} \\
 &\quad + \dot{q}_0 / k m^2 dx \\
 &\quad + h A_c \theta_L
 \end{aligned}$$

It becomes

$$\begin{aligned}
 \dot{q}_{\text{loss}} &= \frac{hP}{m} \left[ -\frac{h \theta_L}{kL} + \left[ \theta_0 - \frac{\dot{q}_0}{m^2 k} \right] \tanh(mL) \right. \\
 &\quad \left. + \frac{h \theta_L}{k m \cosh mL} \right] + \dot{q}_0 A_L + h A_c \theta_L
 \end{aligned}$$

Ans.

(C)

$$\left. \frac{dT}{dx} \Big|_{x=0} = 0 \rightarrow \frac{d\theta}{dx} \Big|_{x=0} = 0 \right\}$$

$$\left. \theta = c_1 e^{mx} + c_2 e^{-mx} + \frac{\dot{q}_0}{m^2 k} \right\} \rightarrow c_1 m - c_2 m = 0$$

$$\text{and } \dot{q}_0 = hP/A \left[ \theta_0 + \frac{h \theta_L}{k m \sinh(mL)} \right] \text{ Ans.}$$

Problem 2.

$$(a) \quad Bi = \frac{hL_c}{k}$$

$$L_c = \frac{V}{A_s}$$

$$V = [39 \times 24 \times 12] - 15 \times 6 \times 24 - \frac{\pi}{4} (16)^2 \times 12 = 6.659 \times 10^{-6} \text{ m}^3$$

$$A = 3 \times 24 \times 12 + 2 \times 15 \times 6 + 2 \times 24 \times 6 + 2 \times 39 \times 24 \\ - 2 \times \frac{\pi}{4} (16)^2 + \pi \times 16 \times 12 = 3.405 \times 10^{-3} \text{ m}^2$$

$$\rightarrow L_c = \frac{6.659 \times 10^{-6}}{3.405 \times 10^{-3}} = 1.9556 \times 10^{-3} = 1.95 \text{ mm}$$

$$\rightarrow Bi = \frac{25 \times 0.00195}{18.9} = 2.58 \times 10^{-3} < 0.1 \quad \text{lumped cap. is valid}$$

$$(b) \quad Fo = \frac{\alpha t}{L_c^2} = \frac{\left(\frac{k}{\rho c_p}\right) t}{L_c^2} = \frac{\left(\frac{18.9}{7978 \times 559}\right) t}{(1.9556 \times 10^{-3})^2} = 1.1081 \times t$$

and

$$\frac{\theta}{\theta_i} = \exp(-Bi \times Fo)$$

$$\text{or } \frac{54 - 30}{600 - 30} = \exp(-2.58 \times 10^{-3} \times 1.1081 \times t)$$

$$\rightarrow t = 1107.97 \text{ Sec.} = 18.4 \text{ min} \quad \text{Ans.}$$

Prob 2. / cont'd.

$$(c) \underset{\text{conv.}}{q} = h A_s (T - T_{\infty})$$

$$= 25 \times 3.405 \times 10^{-3} \times (54 - 30) = 2.043 \text{ W} \quad \text{Ans.}$$

$$q = -mc \frac{dT}{dt}, \quad m = \rho V$$

$$\rightarrow \frac{dT}{dt} = \frac{-q}{mc} = \frac{-2.043}{7978 \times 6.65 \times 10^6 \times 559} = -6.88 \times 10^{-2} \text{ K/s}$$

Ans.